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EXAMINER

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Please find below and/or attached an Office communication concerning this application or proceeding.

The time period for reply, if any, is set in the attached communication.

DETAILED ACTION

Claim Rejections - 35 USC § 102

The following is a quotation of the appropriate paragraphs of 35 U.S.C. 102 that form the basis for the rejections under this section made in this Office action:

A person shall be entitled to a patent unless –

(b) the invention was patented or described in a printed publication in this or a foreign country or in public use or on sale in this country, more than one year prior to the date of application for patent in the United States.

Claims 1-8, 17-18, 20-21, 23, and 25 are rejected under 35 U.S.C. 102(b) as being anticipated by Anderson (US 3,051,639).

Regarding claim 1, Anderson discloses a reactor for the production of nanoparticles in an aerosol process comprising: (a) a reaction chamber having a wall, an inlet and an outlet the inlet for introducing a hot carrier gas to the reaction chamber which hot carrier gas flows from the inlet through the reaction chamber and out the outlet, (b) a quench zone located downstream of the reaction chamber having an inlet and an outlet, (c) one or more quench inlets being positioned approximately about the outlet of the reaction chamber for introducing a quench material, (d) one or more reactant inlets positioned between the reaction chamber inlet and the quench inlets for introducing one or more reactants; the reaction chamber comprising: (i) a spacer zone having a length, $L_{sub.1}$, extending from the reaction chamber inlet and ending approximately about the reactant inlets and (ii) a homogenization zone having a length $L_{sub.2}$ extending from approximately the location of the reactant inlets and ending approximately about the quench zone inlet; the spacer zone for allowing the hot carrier gas to carry the reactants to the homogenization zone, the homogenization zone for

contacting the reactants under conditions suitable for forming a reaction product and passing the reaction product to the quench zone, L.sub.1 being sufficient for the hot carrier gas to attach to the wall of the spacer zone of the reaction chamber prior to the reactant inlets and L.sub.2 being sufficient for a residence time of the reactants within the homogenization zone suitable for forming the reaction product which when withdrawn from the outlet of the quench zone is a nanoparticle (see column 1, lines 8-47 and line 71 through column 2, line 21; and figure 1) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, and the quench zone is element 30.

Claims 2-5 depend on claim 1 such that the reasoning used to reject claim 1 will be used to reject the dependent portions of the claims.

Regarding claim 2, Anderson discloses a reactor which further comprises a high temperature heating means for heating the carrier gas selected from the group consisting of a DC plasma arc, RF plasma, electric heating, conductive heating, flame reactor and laser reactor (see column 1, lines 8-27 and line 71 through column 2, line 21).

Regarding claim 3, Anderson discloses a reactor which further comprises a DC plasma arc for heating the carrier gas (see column 1, lines 8-27 and line 71 through column 2, line 21).

Regarding claim 4, Anderson discloses a reactor which further comprises an RF plasma for heating the carrier gas (see figure 1 and column 1, lines 40-48)

Regarding claim 5, Anderson discloses a reactor wherein the reaction chamber further comprises a homogenizer which provides the spacer zone and the homogenization zone (see column 1, lines 8-47 and figure 1) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, and the quench zone is element 30.

Claims 6-7 depend on claim 5 such that the reasoning used to reject claim 5 will be used to reject the dependent portions of the claims.

Regarding claim 6, Anderson discloses a reactor wherein the homogenizer is constructed of copper or ceramic material (See column 2, lines 27-30).

Regarding claim 7, Anderson discloses a reactor wherein the homogenizer has a wall, an entrance and an exit, the homogenizer wall converging to a nozzle tip at the exit which is spaced a distance $L_{sub.1} + L_{sub.2} + L_{sub.3}$ from the entrance (see figure 3) the homogenizer begins where the arc gas enters the reactor chamber and ends just before the entry of water at entry 80.

Claim 8 depends on claim 7 such that the reasoning used to reject claim 7 will be used to reject the dependent portions of the claims.

Regarding claim 8, Anderson discloses a reactor in which the distance $L_{sub.3}$ is zero (see figure 3) the homogenizer begins where the arc gas enters the reactor chamber and ends just before the entry of water at entry 80.

Regarding claim 17, Anderson discloses a reaction chamber for minimizing flow recirculation in a reactor, the reaction chamber comprising a wall, an entrance and an exit wherein, in the vicinity of the exit, the wall of the homogenizer converges to a nozzle tip from which a reaction product can be withdrawn, a hot carrier gas inlet located about the entrance of the reaction chamber and quench material inlets located about the exit of the reaction chamber and one or more reactant inlets located between the hot carrier gas inlet and the quench inlets, the homogenizer having (i) a spacer zone having a length, $L_{sub.1}$, extending from the reaction chamber entrance and ending about the reactant inlets and (ii) a homogenization zone having a length $L_{sub.2}$ extending from the reactant inlets to a position downstream of the quench inlets for contacting the hot carrier gas and the reactants and wherein $L_{sub.1}$ of the spacer zone is sufficient for the hot carrier gas to attach to the wall of the reaction chamber before the hot carrier gas reaches the reactant inlets and $L_{sub.2}$ of the reaction chamber being sufficient for a residence time within the homogenization zone suitable for forming the reaction product (see column 1, lines 8-47 and line 71 through column 2, line 21; and figure 1) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, and the quench zone is element 30.

Regarding claim 18, Anderson discloses a reactor for the production of nanoparticles from an aerosol process comprising: (a) a reactor chamber having axially spaced inlet and outlet ends along the reactor axis wherein positioned at the inlet end of the reactor chamber is a high temperature heating means to heat a carrier gas having a flow direction axially from the reaction chamber inlet downstream through the reaction chamber and out the chamber outlet and wherein one or more quench gas inlets are positioned up stream from the outlet end of the reactor chamber for introducing a quench gas for cooling; (b) a reaction chamber having an axially spaced entrance and an exit wherein in the vicinity of the exit, the homogenizer converges to a nozzle tip, the entrance of the homogenizer being aligned with the inlet to the reaction chamber and the homogenizer being inserted within the reaction chamber and held in place by a homogenizer holder such that the homogenizer extends from the inlet end of the reaction chamber securely fitting against the inlet end for at least a portion of the homogenizer's overall length and wherein the homogenizer comprising two zones: (i) a spacer zone having a length, $L_{sub.1}$, extending from the reaction chamber entrance and ending where one or more reactant inlet tubes are positioned, after having passed through a wall of the reaction chamber, to deliver one or more reactants into the reaction chamber so the reactants contact the hot carrier gas and (ii) a homogenization zone extending from the reactant inlet tubes' location to a position down stream of the quench gas inlets; and wherein carrier gas and reactants mix and react in the homogenization zone and pass through the flow homogenization exit nozzle to enter a quench zone of the reaction chamber defined by the quench gas inlet location in a

reaction chamber wall and the reaction chamber outlet and wherein L.sub.1 of the spacer zone must be long enough to have the hot gas flow attached to walls of the reaction chamber before the hot gas reaches the reactant inlets and the overall length (L.sub.1+L.sub.2) of the reaction chamber is designed to a residence time sufficient that the following three tasks are completed before gas flow exiting the homogenizer: (1) gas flow in the reaction chamber has achieved a near one-dimensional flow and concentration profile; and (2) gas-phase nucleation of product particles has been initiated (see column 1, lines 8-47 and line 71 through column 2, line 21; and figures 1 and 3) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, the homogenizer begins where the arc gas enters the reactor chamber and ends just before the entry of water at entry 80, and the quench zone is element 30.

Regarding claim 20, Anderson discloses a reaction chamber for minimizing flow recirculation in a reactor, the reaction chamber comprising an axially spaced entrance and an exit wherein in the vicinity of the exit the homogenizer converges to nozzle tip, the entrance of the homogenizer being aligned with the inlet to the reaction chamber and the homogenizer being inserted within the reaction chamber and held in place by a homogenizer holder such that the homogenizer extends from the inlet end of the reaction chamber securely fitting against the inlet end for at least a portion of the homogenizer's overall length and wherein the homogenizer comprising two zones: (i) a spacer zone having a length, L.sub.1, extending from the reaction chamber entrance

and ending where one or more reactant inlet tubes are positioned, after having passed through a wall of the reaction chamber, to deliver one or more reactants into the reaction chamber so the reactants contact the hot carrier gas and (ii) a homogenization zone extending from the reactant inlet tubes' location to a position down stream of the quench gas inlets; and wherein carrier gas and reactants mix and react in the homogenization zone and pass through the flow homogenization exit nozzle wherein L.sub.1 of the spacer zone must be long enough to have the hot gas flow attached to walls of the reaction chamber before the hot gas reaches the reactant inlets and the overall length (L.sub.1+L.sub.2) of the reaction chamber is designed to a residence time sufficient that before gas flow exits the homogenizer: gas flow in the reaction chamber has achieved a near one-dimensional flow and concentration profile (see column 1, lines 8-47 and line 71 through column 2, line 21; and figures 1 and 3) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, the homogenizer begins where the arc gas enters the reactor chamber and ends just before the entry of water at entry 80, and the quench zone is element 30.

Regarding claim 21, Anderson inherently discloses that the reaction chamber reduces gas and particle entrainment in the reactant inlet region and promotes efficient mixing on the homogenization reaction (see figure 1).

Regarding claim 23, Anderson discloses that the reactor is a subsonic reactor (see column 5, lines 16-22).

Regarding claim 25, Anderson inherently discloses that the location of the reactant inlets downstream of the spacer zone provide a reactant injection site that avoids exposing the reactants to a flow recirculation induced by the hot carrier gas flowing out the outlet (See figure 1).

Claim Rejections - 35 USC § 103

The following is a quotation of 35 U.S.C. 103(a) which forms the basis for all obviousness rejections set forth in this Office action:

(a) A patent may not be obtained though the invention is not identically disclosed or described as set forth in section 102 of this title, if the differences between the subject matter sought to be patented and the prior art are such that the subject matter as a whole would have been obvious at the time the invention was made to a person having ordinary skill in the art to which said subject matter pertains. Patentability shall not be negated by the manner in which the invention was made.

The factual inquiries set forth in *Graham v. John Deere Co.*, 383 U.S. 1, 148 USPQ 459 (1966), that are applied for establishing a background for determining obviousness under 35 U.S.C. 103(a) are summarized as follows:

1. Determining the scope and contents of the prior art.
2. Ascertaining the differences between the prior art and the claims at issue.
3. Resolving the level of ordinary skill in the pertinent art.
4. Considering objective evidence present in the application indicating obviousness or nonobviousness.

This application currently names joint inventors. In considering patentability of the claims under 35 U.S.C. 103(a), the examiner presumes that the subject matter of the various claims was commonly owned at the time any inventions covered therein were made absent any evidence to the contrary. Applicant is advised of the obligation under 37 CFR 1.56 to point out the inventor and invention dates of each claim that was not commonly owned at the time a later invention was made in order for the examiner to consider the applicability of 35 U.S.C. 103(c) and potential 35 U.S.C. 102(e), (f) or (g) prior art under 35 U.S.C. 103(a).

Claims 19, 22, and 24 are rejected under 35 U.S.C. 103(a) as being unpatentable over Anderson (US 3,051,639).

Regarding claim 19, Anderson discloses an aerosol process for producing nanosize particles, comprising the steps: (a) introducing a carrier gas into a reactor chamber having (i) axially spaced inlet and outlet ends along the reactor axis wherein positioned at the inlet end of the reactor chamber is a high temperature heating means to heat a carrier gas having a flow direction axially from the reaction chamber inlet downstream through the reaction chamber and out the chamber outlet and wherein one or more quench gas inlets are positioned up stream from the outlet end of the reactor chamber for introducing a quench gas for cooling; and (ii) a reaction chamber having an axially spaced entrance and an exit wherein in the vicinity of the exit, the homogenizer converges to nozzle tip, and wherein the homogenizer comprising two zones: (i) a spacer zone having a length, $L_{sub.1}$, extending from the reaction chamber entrance and ending where one or more reactant inlet tubes are positioned, after having passed

through a wall of the reaction chamber, to deliver one or more reactants into the reaction chamber so the reactants contact the hot carrier gas and (ii) a homogenization zone extending from the reactant inlet tubes' location to a position down stream of the quench gas inlets; and wherein carrier gas and reactants mix and react in the homogenization zone and pass through the flow homogenization exit nozzle to enter a quench zone of the reaction chamber defined by the quench gas inlet location in a reaction chamber wall and the reaction chamber outlet and wherein L.sub.1 of the spacer zone must be long enough to have the hot gas flow attached to walls of the reaction chamber before the hot gas reaches the reactant inlets and the overall length (L.sub.1+L.sub.2) of the reaction chamber is designed to a residence time sufficient that the following three tasks are completed before gas flow exiting the homogenizer: (1) gas flow in the reaction chamber has achieved a near one-dimensional flow and concentration profile; and (2) gas-phase nucleation of product particles has been initiated; (b) heating the carrier gas by thermal contact with the heating means to a temperature to initiate reaction of the carrier gas with one or more reactants; (c) introducing one or more reactants through the reactant inlet tubes to form a reaction mixture; (d) adjusting flow rates of the carrier gas and reactants such that reaction mixture flows through the flow homogenization chamber at a rate such that (1) flow of the reaction mixture is characterized by one-dimensional flow and a one-dimensional concentration profile; and (2) gas-phase nucleation of the product has been initiated; (e) immediately injecting quench gas through the quench gas inlet tubes as the reaction mixture flow enters the quench zone so that particle coagulation and coalescences is

reduced and temperature of the reaction mixture and product is decreased; and (f) separating and collecting the product (see column 1, lines 8-47 and line 71 through column 3, line 40; column 4, lines 30-60; and figures 1 and 3) where the spacer zone is the area of the reactor chamber from where the arc gas enter to the point before the fluid hydrocarbon enters, the homogenization zone is the area of the reactor chamber from the entry of the fluid hydrocarbon until the exit of the product, the homogenizer begins where the arc gas enters the reactor chamber and ends just before the entry of water at entry 80, and the quench zone is element 30.

Anderson does not disclose the homogenizer entrance being aligned with the inlet to the reaction chamber and the homogenizer being inserted within the reaction chamber and held in place by a homogenizer holder such that the homogenizer extends from the inlet end of the reaction chamber securely fitting against the inlet end for at least a portion of the homogenizer's overall length.

It would have been obvious to one having ordinary skill in the art at the time the invention was made to make the homogenizer separable from the reactor chamber, since it has been held that constructing a formerly integral structure in various elements involves only routine skill in the art.

Regarding claim 22, Anderson does not disclose that the reaction chamber comprises a straight region and a convergent section in figure 1.

However, in figure 3 Anderson discloses the reaction chamber comprises a straight region and a convergent section.

Therefore, because these two reaction chambers were art-recognized equivalents at the time the invention was made, one of ordinary skill in the art would have found it obvious to substitute the reaction chamber comprises a straight region and a convergent section for a straight reaction chamber.

Regarding claim 24, Anderson does not disclose the hot carrier gas which flows out the outlet has a gas pressure at the outlet in the range of 1-5 atmospheres.

It would have been obvious to one having ordinary skill in the art at the time the invention was made to have the hot carrier gas which flows out the outlet has a gas pressure at the outlet in the range of 1-5 atmospheres, since it has been held that where the general conditions of a claim are disclosed in the prior art, discovering the optimum or workable ranges involves only routine skill in the art (see MPEP 2144.05 (II-A)).

Response to Arguments

Applicant's arguments filed September 3, 2008 have been fully considered but they are not persuasive.

In response to applicant's arguments, the recitation of a reactor for the production of nanoparticles has not been given patentable weight because the recitation occurs in the preamble. A preamble is generally not accorded any patentable weight where it merely recites the purpose of a process or the intended use of a structure, and where the body of the claim does not depend on the preamble for completeness but, instead, the process steps or structural limitations are able to stand alone. See *In re Hirao*, 535

F.2d 67, 190 USPQ 15 (CCPA 1976) and *Kropa v. Robie*, 187 F.2d 150, 152, 88 USPQ 478, 481 (CCPA 1951).

In response to applicant's argument that the spacer zone for allowing the hot carrier gas to carry the reactants to the homogenization zone, the homogenization zone for contacting the reactants under conditions suitable for forming a reaction product and passing the reaction product to the quench zone, L.sub.1 being sufficient for the hot carrier gas to attach to the wall of the spacer zone of the reaction chamber prior to the reactant inlets and L.sub.2 being sufficient for a residence time of the reactants within the homogenization zone suitable for forming the reaction product which when withdrawn from the outlet of the quench zone is a nanoparticle, a recitation of the intended use of the claimed invention must result in a structural difference between the claimed invention and the prior art in order to patentably distinguish the claimed invention from the prior art. If the prior art structure is capable of performing the intended use, then it meets the claim.

Applicant's arguments, see Remarks, filed September 3, 2008, with respect to objections of the specification and claims 18-20 have been fully considered and are persuasive. The objections of the specification and claims 18-20 have been withdrawn.

Conclusion

THIS ACTION IS MADE FINAL. Applicant is reminded of the extension of time policy as set forth in 37 CFR 1.136(a).

A shortened statutory period for reply to this final action is set to expire THREE MONTHS from the mailing date of this action. In the event a first reply is filed within TWO MONTHS of the mailing date of this final action and the advisory action is not mailed until after the end of the THREE-MONTH shortened statutory period, then the shortened statutory period will expire on the date the advisory action is mailed, and any extension fee pursuant to 37 CFR 1.136(a) will be calculated from the mailing date of the advisory action. In no event, however, will the statutory period for reply expire later than SIX MONTHS from the mailing date of this final action.

Any inquiry concerning this communication or earlier communications from the examiner should be directed to NATASHA YOUNG whose telephone number is 571-270-3163. The examiner can normally be reached on Mon-Thurs 7:30 am-6:00 pm.

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Walter Griffin can be reached on 571-272-1447. The fax phone number for the organization where this application or proceeding is assigned is 571-273-8300.

Information regarding the status of an application may be obtained from the Patent Application Information Retrieval (PAIR) system. Status information for published applications may be obtained from either Private PAIR or Public PAIR. Status information for unpublished applications is available through Private PAIR only. For more information about the PAIR system, see <http://pair-direct.uspto.gov>. Should you have questions on access to the Private PAIR system, contact the Electronic Business Center (EBC) at 866-217-9197 (toll-free). If you would like assistance from a USPTO Customer Service Representative or access to the automated information system, call 800-786-9199 (IN USA OR CANADA) or 571-272-1000.

/N. Y./
Examiner, Art Unit 1797

/Walter D. Griffin/
Supervisory Patent Examiner, Art Unit 1797